

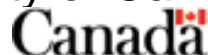
Biomass/Cellulosic Energy Research at Guelph

Transforming Biomass for the Bioeconomy

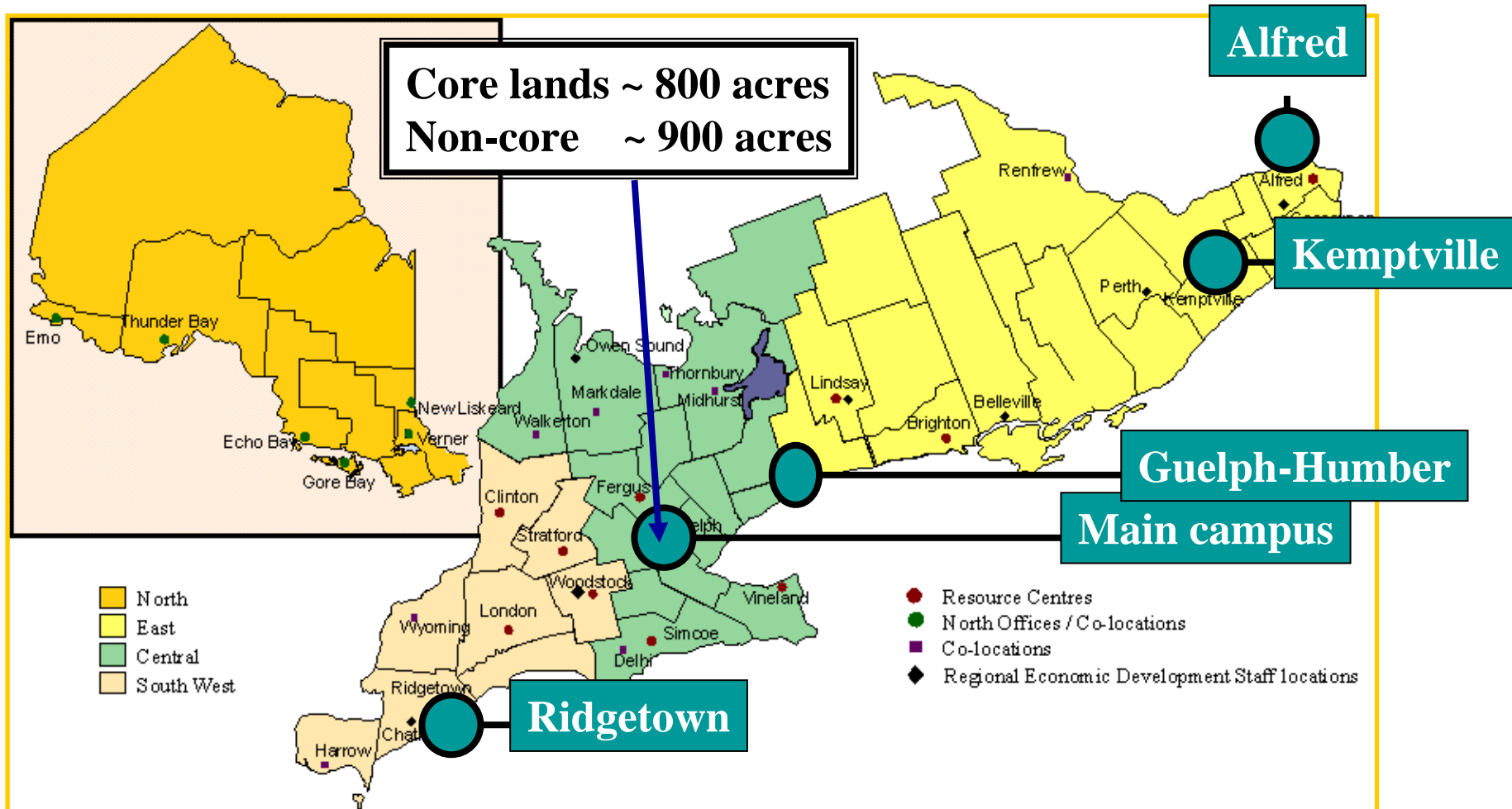
Steven N. Liss, PhD

Associate Vice-President, Research Services
University of Guelph, Guelph, Ontario Canada

University of California – *System-Wide Technology Transfer Forum April 3, 2008*

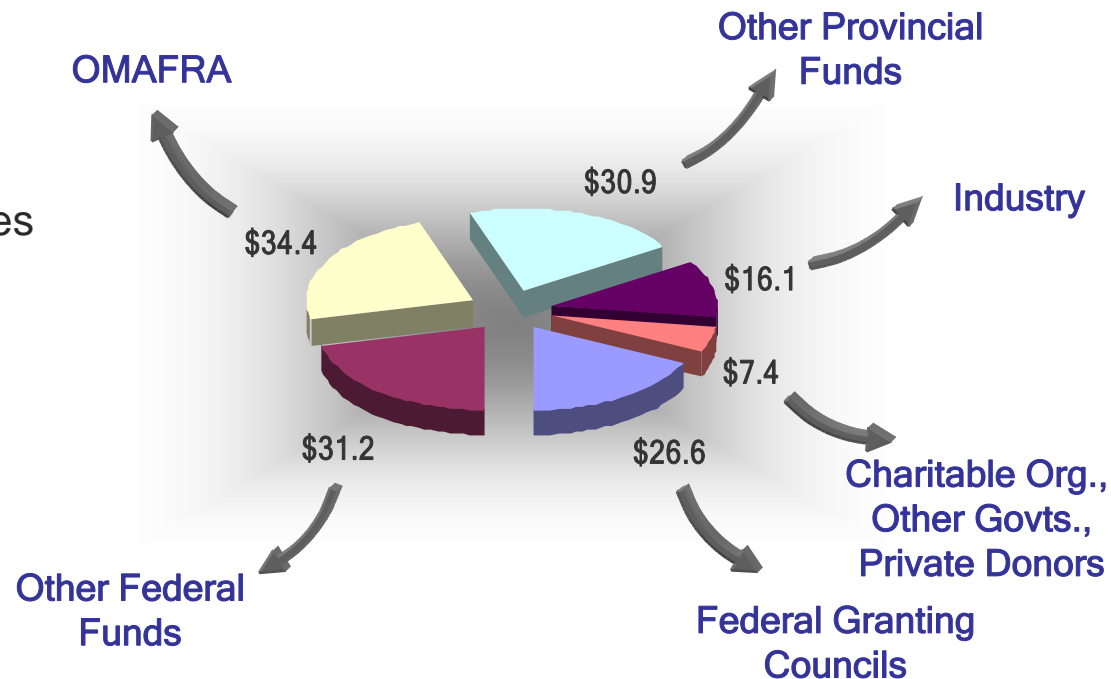
 Canadian Consulate General, San Francisco
Hyatt Regency San Francisco Airport, Burlingame, California

Large Geographic Spread



Facts and Figures

- **Institutional revenue**
 - ~\$ 510 million
- **Research support**
 - ~ \$145 million
- **Undergraduate students**
 - 16,000 - Guelph campus
 - 2,500 - Guelph-Humber
- **Diploma students**
 - 1,000 - Regional campuses
- **Graduate students**
 - 2,000 - Guelph campus
- **Distance Education**
 - > 51,000 registrants
- **Faculty**
 - ~800
- **Staff**
 - ~1,900



▪ UG/OMAFRA partnership returns \$3 for every \$1 received in the form of various impacts. The annual economic impact exceeds \$1.15 billion

Deloitte and Touche LLP UG/OMAFRA Impact Study 2007

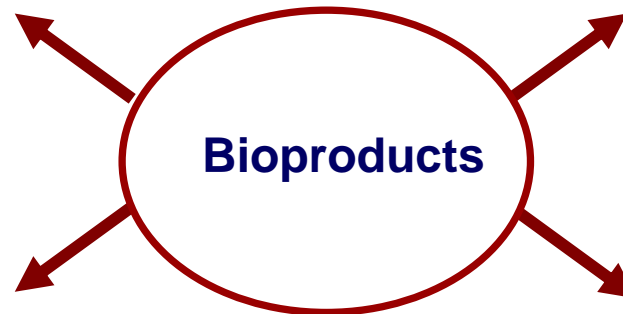
Agriculture, Life Sciences, Physical and Engineering Sciences

Energy

Biodiesel from crop oils
Ethanol from ligno-cellulose
Biogas, cogeneration

Food and Agri-Forestry

Crop breeding/biotech
Livestock nutrition
Production systems, environment



Health and Nutrition

Omega 3 in dairy products, etc.
Probiotics in eggs and milk
Clinical trials on functional foods

Industrial-Manufacturing

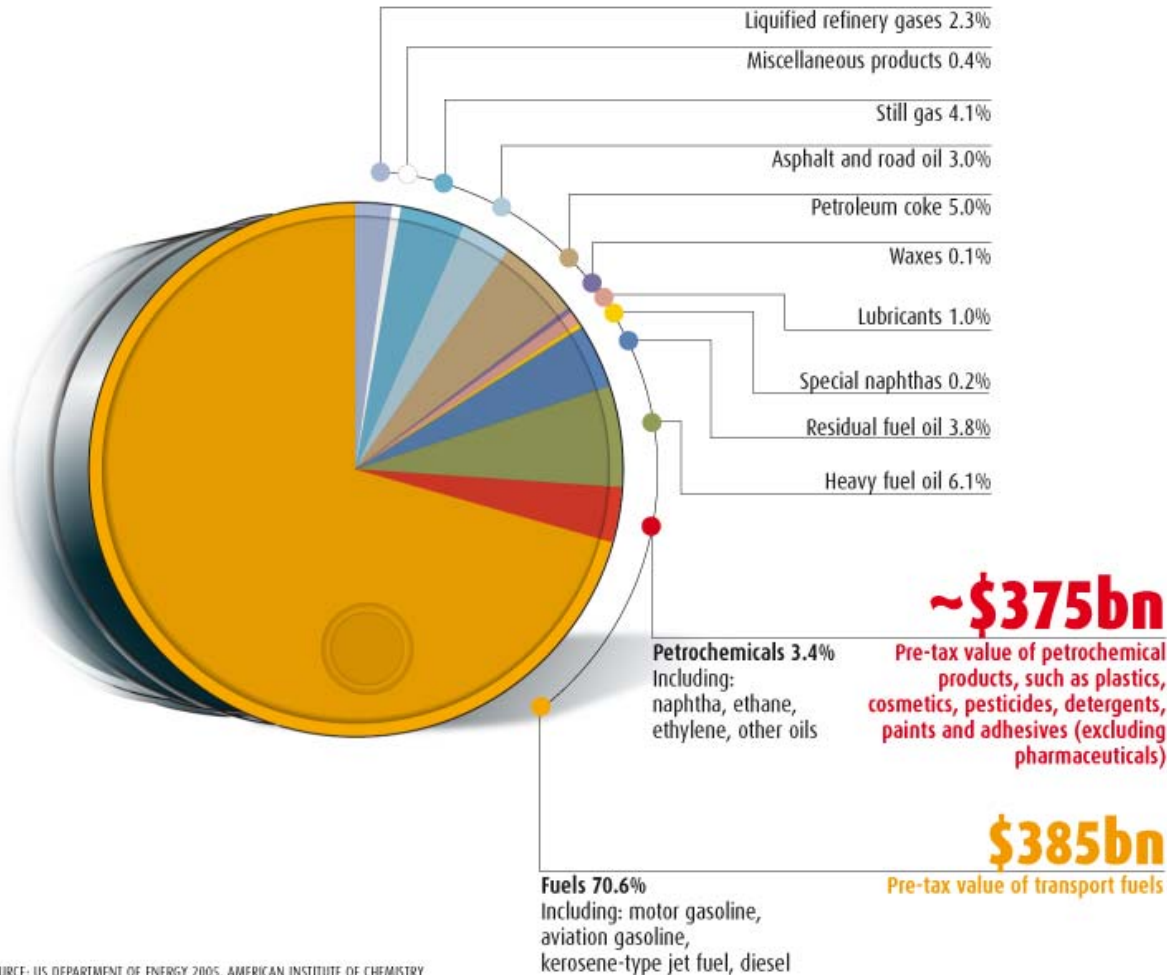
BioCar (Premier's Research Chair)
Polylactic Acid
Construction materials

Producing Chemical Feedstock from Biomass

CHANGING LIVES
IMPROVING LIFE

OIL BARREL BREAKDOWN

Despite consuming a small fraction of US oil compared with fuel, petrochemical products are worth more



SOURCE: US DEPARTMENT OF ENERGY 2005, AMERICAN INSTITUTE OF CHEMISTRY

Source: *New Scientist* 2007

- Only ~ 3.4 % of all crude oil processed ends up in petrochemicals – over 70 % is used as fuel, the remaining goes towards asphalt, coke, bitumen, wax, and other products.
- **In spite of this, these chemicals are worth as much as the fuel !**
- Because the total volume of material is comparatively small there is little competition with food production ...



Ontario **BioCar** Initiative

Goal

Accelerate the use of biomass in automotive materials, while maintaining or improving value

Focus

Replacement of petroleum-based products by biochemicals and high content bio-fibre materials, from the field and forests

UNIVERSITY
of GUELPH



WINDSOR

Ontario **Bio**
Car
Initiative

Project

Genes to Fields: Corn Biotechnology Capacity for Ontario

Background

- Corn is one of the world's most important food crops
- More recently, corn became the foundation of a new "green" economy (renewable corn-based ethanol and industrial polymers)
- Need to to make corn production more profitable and sustainable
- Annual corn production in Ontario is worth \$1 billion

Goal

Test genes that hold the potential to:

- 1. increase yields of corn food/fibre,**
- 2. combat farmer losses caused by Ontario's unpredictable/short-growing seasons, and**
- 3. reduce agricultural greenhouse gas emissions.**

Project

Genes to Fields: Corn Biotechnology Capacity for Ontario

Approach

Corn domestication for adaptation in Northern climates can be accelerated by using modern genetic resources

Established partnership with Syngenta, a leading agbiotech company

\$9M funding from the Ontario Ministry for Research and Innovation, Syngenta, NSERC and the University of Guelph

Research Team

Steven Rothstein (lead PI)
Joseph Colasanti
Elizabeth Lee
Manish Raizada
Matthijs Tollenaar

Lignocellulosic biomass conversion

- Two primary processes:
 - Thermochemical conversion
 - Biochemical conversion (Bioconversion)
- Potential substrates:
 - Agricultural and forestry residues
 - Waste paper and newsprint
 - Dedicated short rotation plants and crops

Four steps in bioconversion

1. Lignocellulosic substrate pretreatment
 - By chemical and physical methods
- 2. Enzyme hydrolysis (*Anthony Clarke*)
 - Cellulases, xylanases & debranching enzymes
- 3. Microbial fermentation (*Hung Lee*)
 - Yeasts and bacteria
4. Co-product development & product recovery

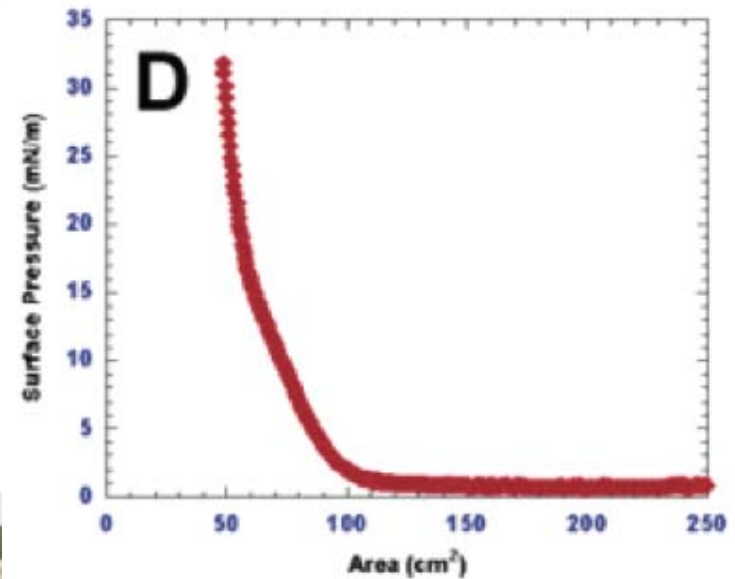
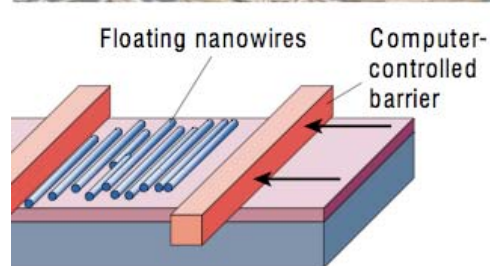
Lignocellulosic biomass conversion is technically feasible, but process economics are poor based on today's technology

Advancing the Development of Cellulase

- **Goal:** *Increase the overall efficiency of the process using genetically modified derivatives of the enzymes (cellulases and cellobiohydrolases) which will include alterations to the carbohydrate-binding modules and their associated tethers.*
- **Key Objectives and Approach**
 - Gain an insight into the binding of cellulolytic enzymes to crystalline cellulose.
 - Both wild-type and engineered enzymes with modified carbohydrate binding modules are being investigated by atomic force microscopy as they bind to and degrade this cellulose.
 - Bacterial cellulose at the moment as a model system to layer it onto a gold surface using the Langmuir-Blodgett technique in an aqueous environment - this has not been done before and Dr. Clarke's group has succeeded.

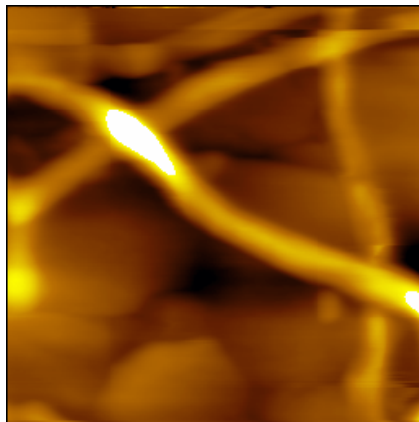
Langmuir-Blodgett

- Logs on a river
 - Use cellulose dispersion
- Order
- Reproducibility

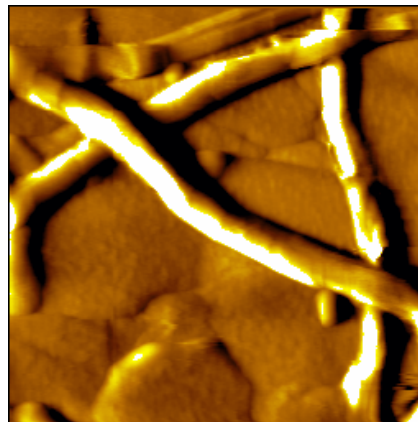


Atomic Force Microscopy

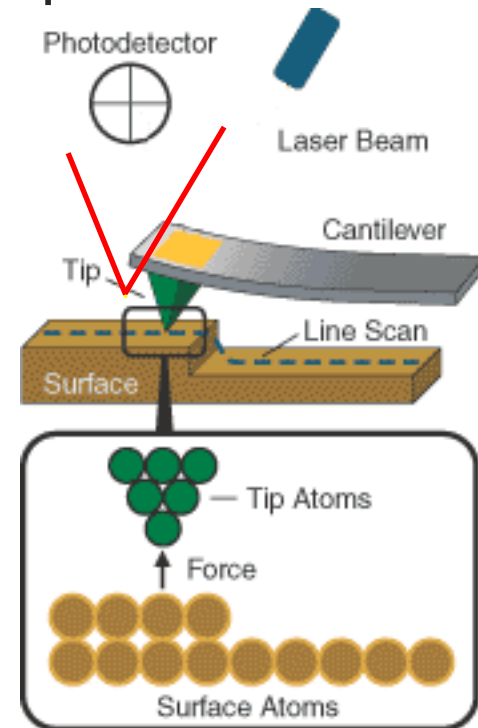
- Soft contact mode
 - Interaction between tip and sample
 - Constant contact
 - Detection modes:
 - Topography
 - Deflection
 - Friction



Topography

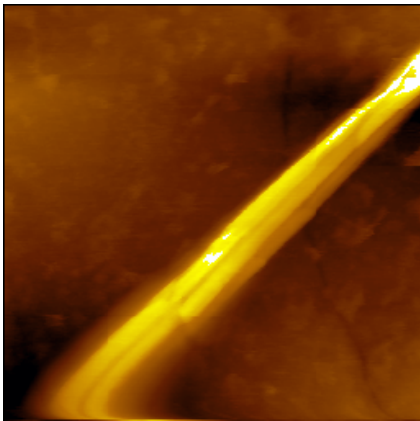


Deflection

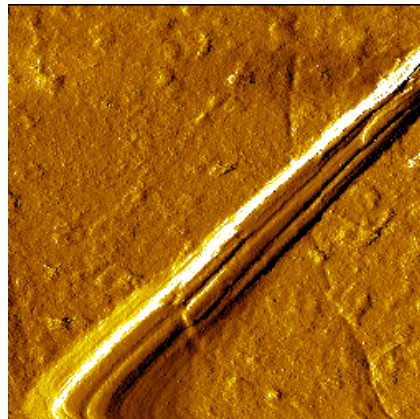


Atomic Force Microscopy

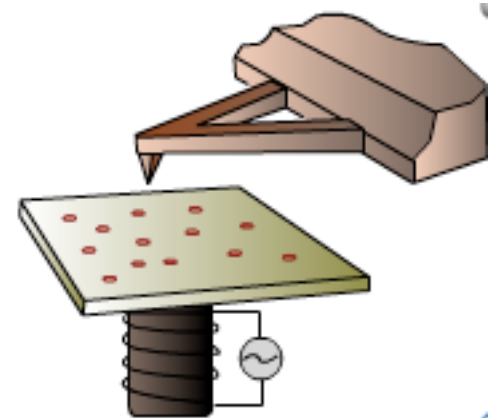
- MAC mode
 - Tip oscillated by applied magnetic field
 - Intermittent contact
 - Ideal for soft samples in liquid environments
 - Detection modes:
 - Topography
 - Amplitude
 - Phase



Topography



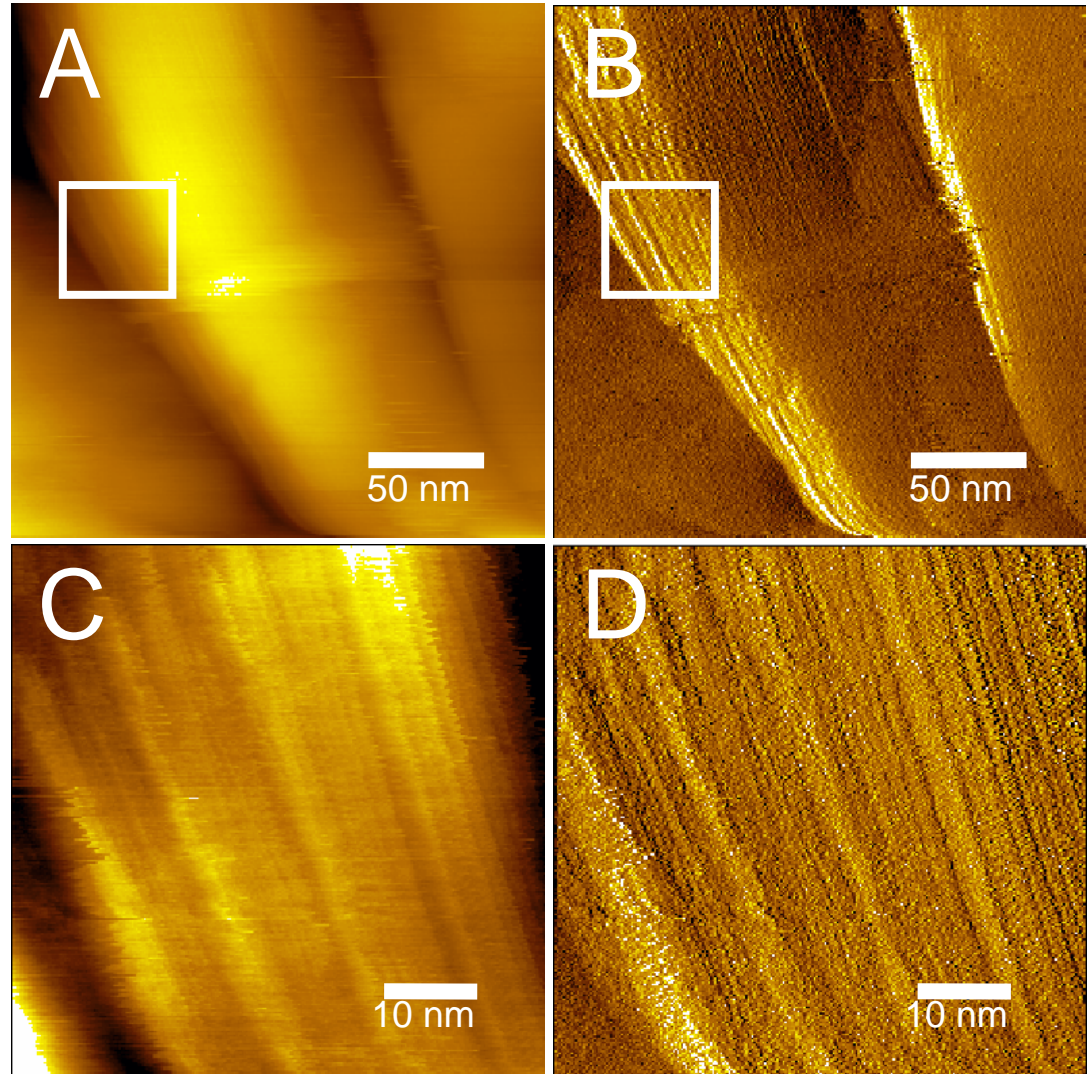
Amplitude



molec.com

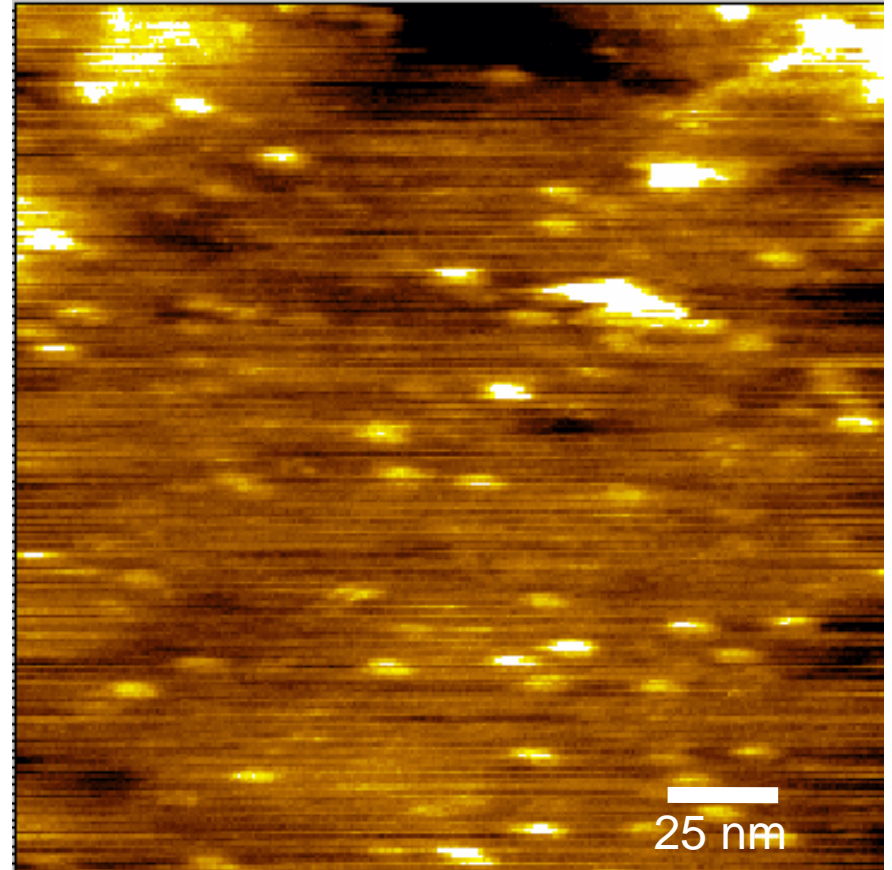
AFM High Resolution

- Soft contact mode
- Cellulose fibers are made up of microfibrils
- Microfibrils 4 nm in diameter



Cellulomonas fimi CenA

- Image CenA on gold to determine size and shape
- MAC mode



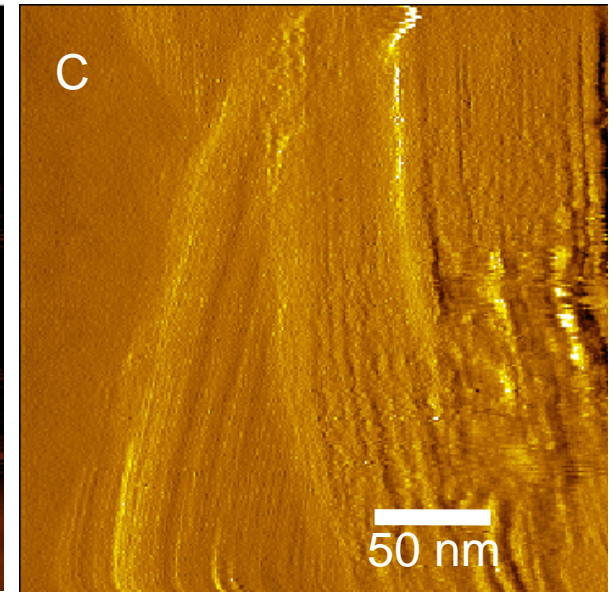
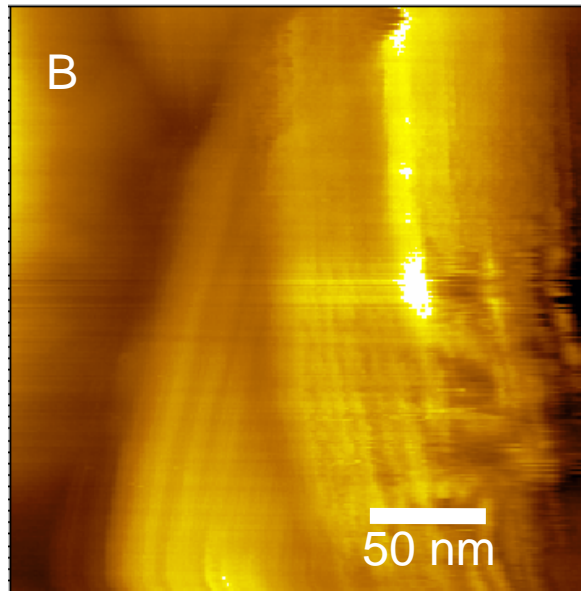
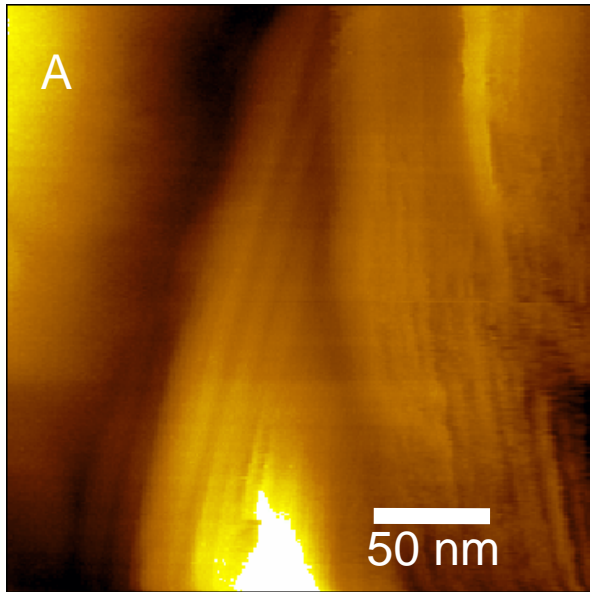
CenA is a bacterial cellulase (beta-1,4-glucanase) comprised of a globular catalytic domain joined to an extended cellulose-binding domain (CBD) by a short linker peptide.

In Situ Degradation with CenA

- MAC mode

Topography

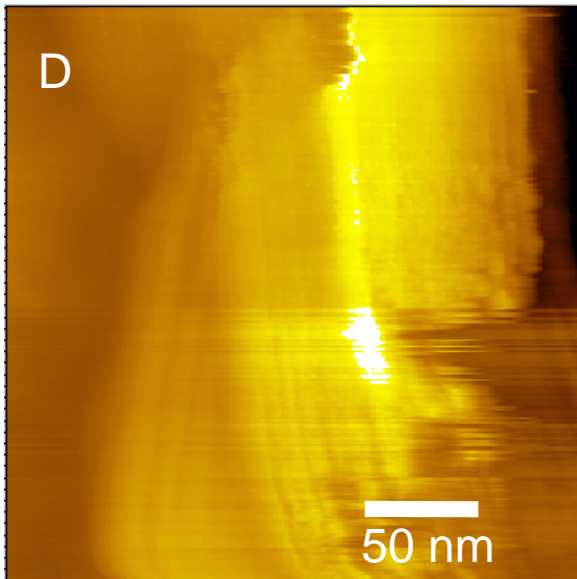
Amplitude



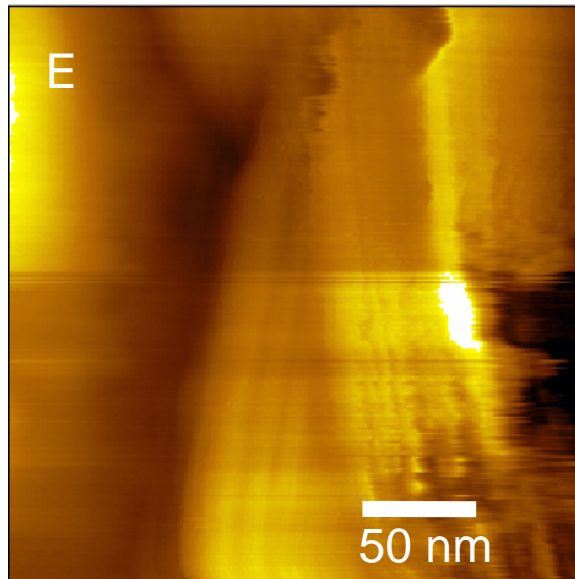
Before enzyme

3 minutes after

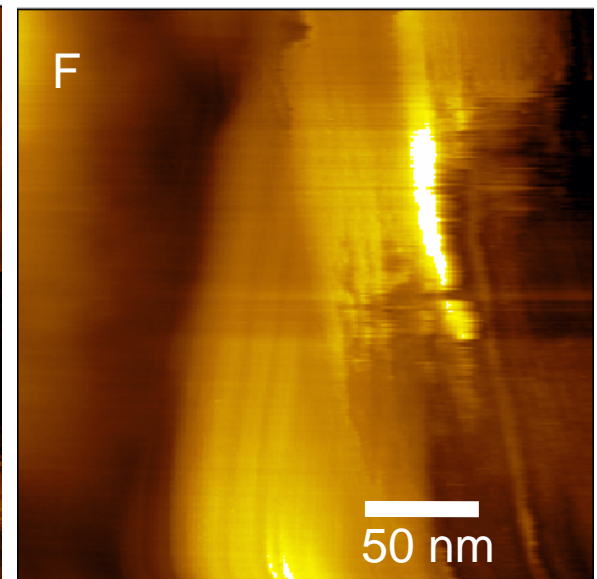
- MAC mode



15 minutes



30 minutes



60 minutes

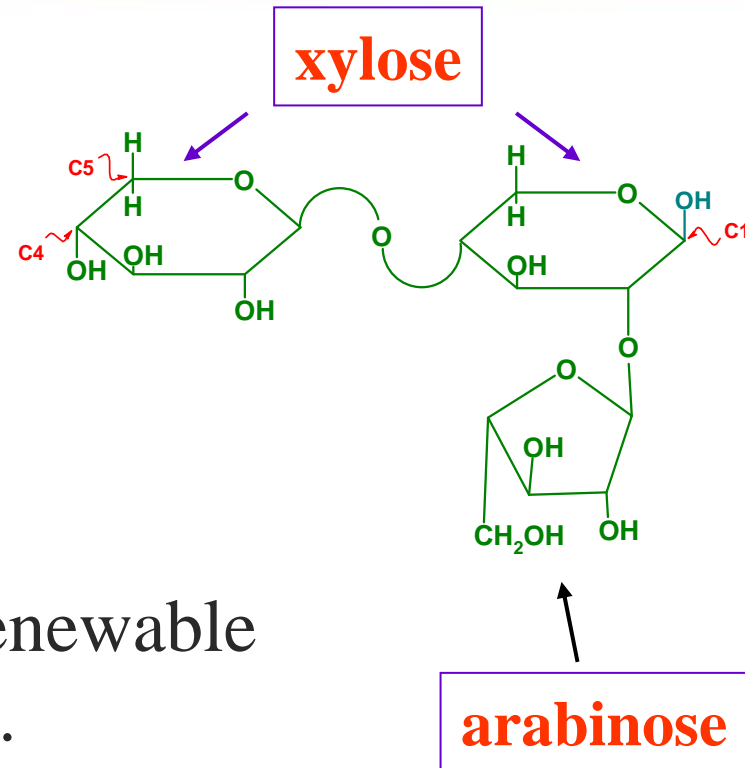
Pentose-Fermenting Yeasts

- **Two main lines of research**
 1. **Biochemistry and physiology of pentose-fermenting yeasts**
 - Researcher: **Hung Lee** (U of Guelph)

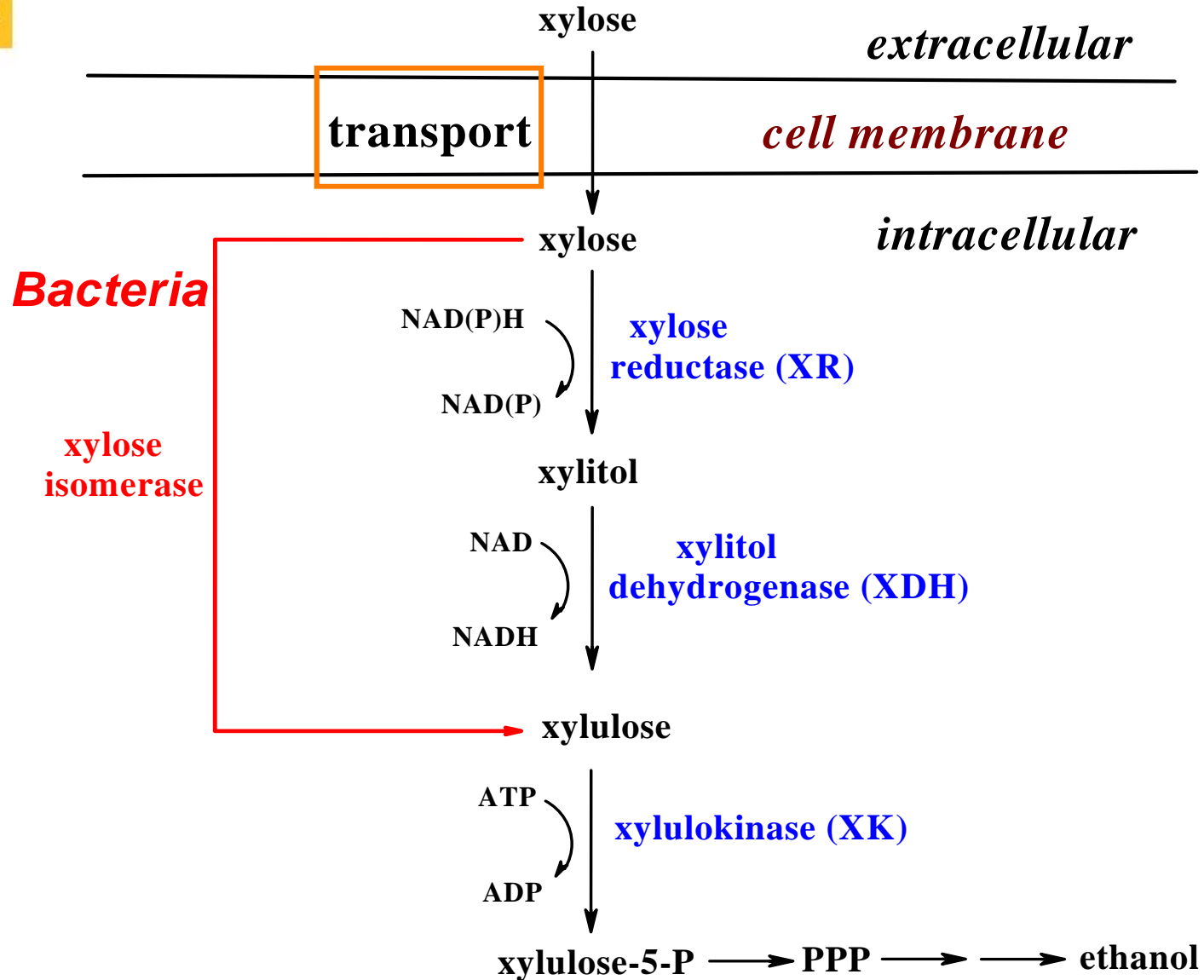
 2. **Genetic improvement of pentose-fermenting yeasts**
 - Researchers: **Hung Lee** (U of Guelph), **Vince Martin** (Concordia U) & **Jack Trevors** (U of Guelph)
 - Partners: **Mike Paice** (FPInnovations – Paprican division) & **Benji Ahvazi** (Tembec)

Pentoses constitute 10-40% of total structural sugars in plant biomass

- **D-xylose.**
 - The second most abundant renewable sugar in nature, after glucose.
- **L-arabinose** is much less abundant than xylose.
- Lignocellulosic biomass sugars also include the hexoses **glucose, mannose and galactose.**



Xylose metabolism in yeasts and fungi



Biochemical studies on xylose reductases

- Focused on the structure-function relationships of yeast xylose reductases.
 - This enzyme is essential for growth of yeasts on xylose
 - This enzyme is inducible by xylose and repressible by glucose and mannose.
- Experimental approaches include site-directed mutagenesis, chemical modification and fluorescence spectroscopy.

Key findings on yeast xylose reductases

- The following 4 catalytic residues were found to be essential for activity: **Asp44, Tyr49, Lys78 & His111**.
- **Lys270** in the IPKS motif was found to be essential for cofactor binding.
- Future studies will examine the structure-function relationships of yeast **xylitol dehydrogenase** and **xylulokinase**.

Genetic improvement of native pentose-fermenting yeasts

- The primary objective is to improve the performance of pentose-fermenting yeasts in industrially relevant lignocellulosic hydrolysates.
- Focus on *Pichia stipitis* for now.
 - Start with UV mutagenesis.
 - Followed by genome shuffling.

Target(s) of genetic improvement

- **Improved tolerance to pretreatment derived inhibitors.**
 - Lignocellulosic substrate being used for selection is a waste pulping liquor known as spent sulfite liquor (SSL) from Tembec.
 - The pulping process generates many inhibitors which adversely affect microbial fermentation.
 - The main inhibitors are acetic acid (from hardwoods), furfurals, hydroxymethyl furfurals, and phenolic compounds.

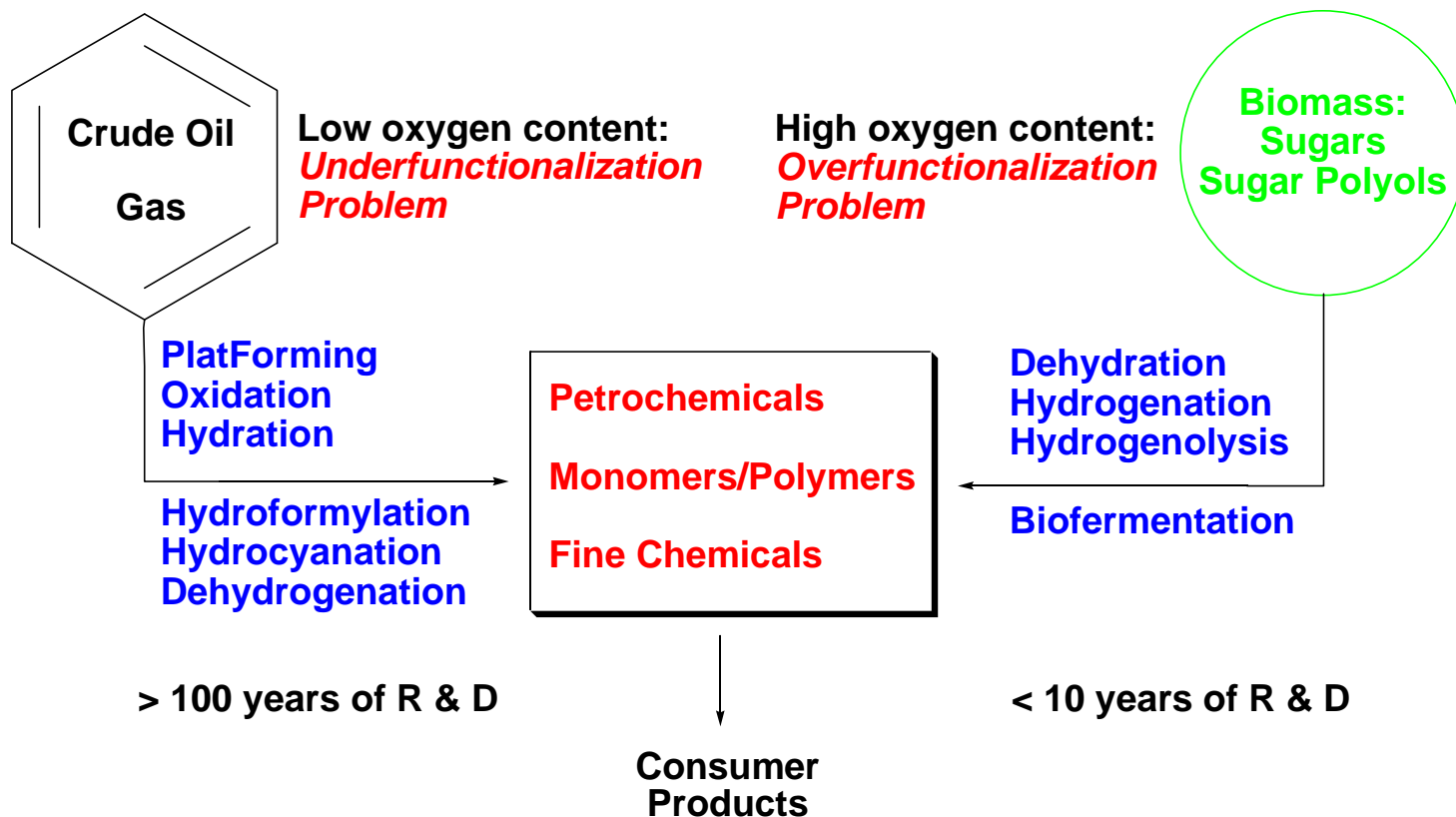
Improved mutants of *Pichia stipitis*

- Selection of improved mutants are based on the following characteristics relative to the wild type (WT)
 - Ability to grow at higher concentrations of hardwood SSL.
 - Ability to grow well on glucose and xylose as the sole carbon source in defined medium, based on growth rate and growth yield measurements.
 - Ability to ferment glucose and xylose individually to ethanol in defined medium in good yield.
 - Better able to ferment a glucose-xylose mixture.

Future targets for genetic improvement

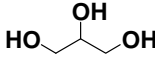
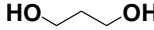
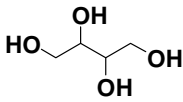

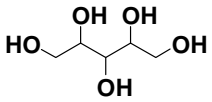
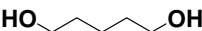
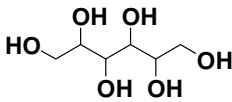

- Simultaneous utilization of glucose and xylose
- Improved ethanol tolerance
- Improved acetic acid tolerance
- Genome shuffling to merge all the improved traits
- Genetic improvement of *Pachysolen tannophilus* and *Candida shehatae*.

The Deoxygenation Challenge



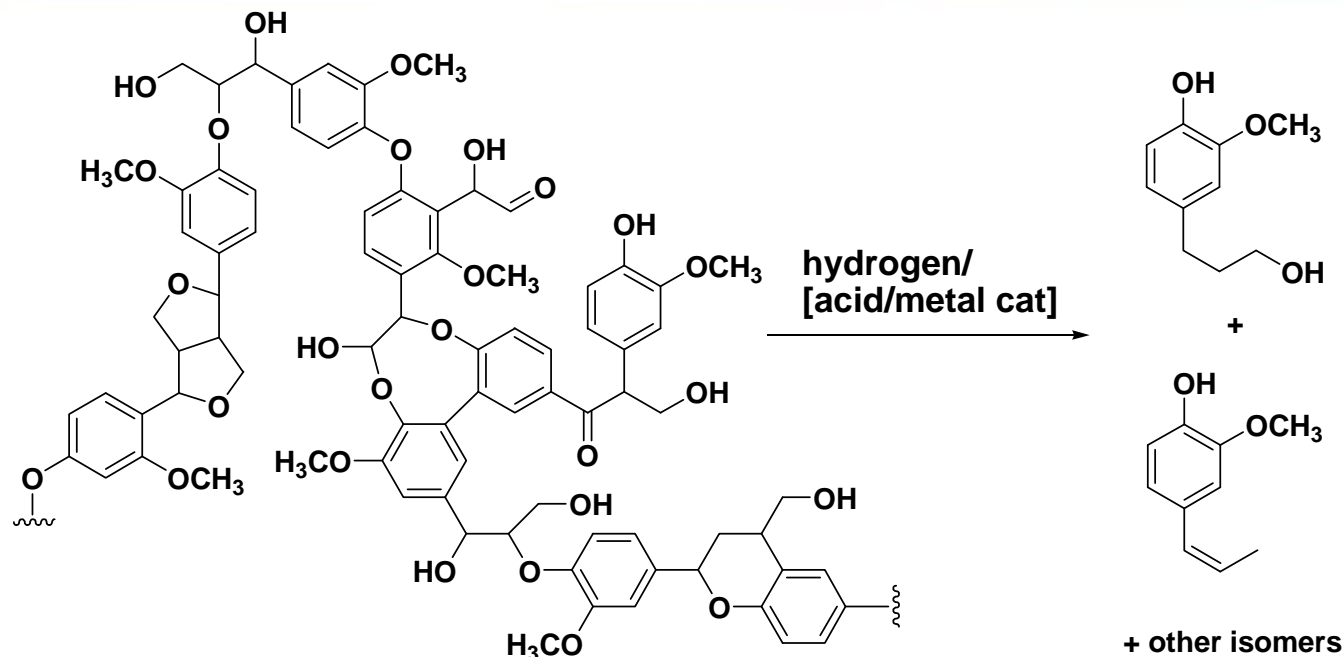
Starting from highly functionalized/oxygenated biomass will require a very different chemical approach than starting from coal/oil/gas ...

Carbon Sources I: Polymers from Sugar Alcohols

	<u>Est. Production 2007 [t/a]:</u>	Biomass	[H ⁺]; - n H ₂ O [cat.]; + n H ₂ (g)	α,ω -diol	Application
C₃	> 1 × 10 ⁶ (and growing → Bio-Diesel glycerol glut ...)		⇌	 1,3-propanediol	Sorona™ (DuPont)/ Corterra™ (Shell)
C₄	? – produced by Cargill as a non-caloric sweetener		⇌	 THF	Lycra™ / Industrial Solvent
C₅	> 25,000 (Xylose) > 30,000 (Xylitol)		⇌	 1,5-pentanediol	Thermoplastic Polyurethanes Polyesters
C₆	> 5,000,000 (glucose) > 600,000 (sorbitol) > 130,000,000 (sucrose)		⇌	 1,6-hexanediol	Polyurethanes Polyesters Potential Nylon-6,6 precursor

Sugar alcohols can provide linear C₃ to C₆ building blocks – ideally α,ω -diols for direct application in polyesters, polyamides and polyurethanes.

Carbon Sources II: Aromatics from Lignins



Typical composition of lignin
(non-sulfonated form)
(Source: Lignin Institute)

- Propyl catechols could serve as platform for epoxy and other resins.
- Combination of aqueous acid digestion with simultaneous hydrogenation/hydrogenolysis could break up lignin framework.
- Steric access to C-O bonds and catalyst deactivation *coking* would not be a problem with homogeneous systems.

Carbon Sources III: Engine Fuel from Bio-Oil

- Obtained by pyrolysis of ligno-cellulosics at $\sim 500\text{ }^{\circ}\text{C}$.
- High viscosity, acidity, water and acid content (15 % w/w formic + acetic acid).
- Hydrogenation upgrade using acid- and water-tolerant iron-based homogeneous catalysts and removal of water formed (by distillation) would lower acid and oxygen content.
→ **3rd generation bio-Diesel**
- Iron catalyst stays in fuel to act as combustion catalyst, i.e., does “double duty” !



200 tons/day

Guelph Plant

A sample of bio-oil obtained by the DYNAMOTIVE process.

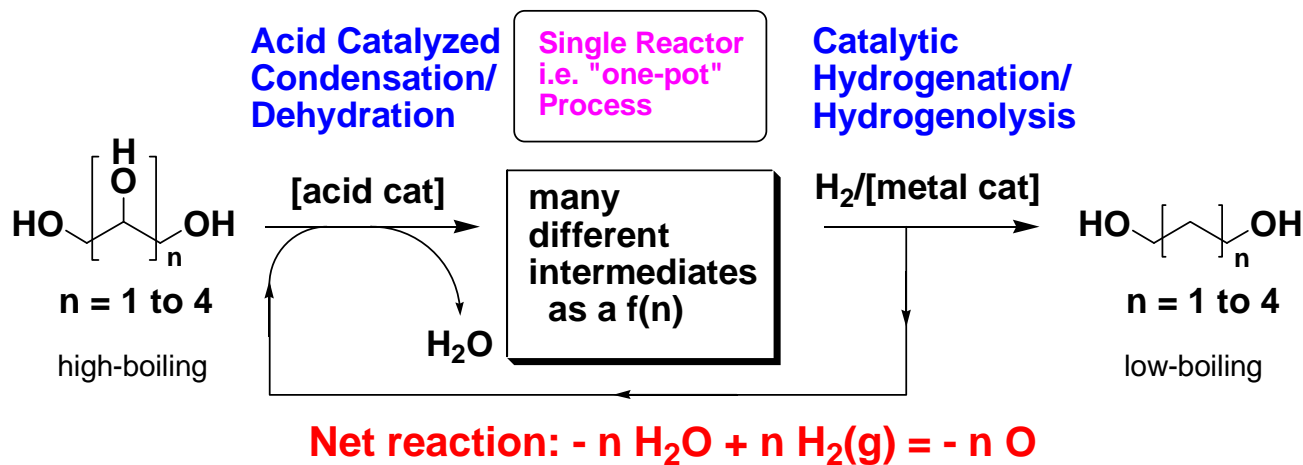
Acidity: pH \sim 2

Oxygen content: \sim 50 % w/w

Water content: \sim 20 % w/w

Not suitable as engine fuel “as is”.

Strategy or How to deoxygenate stuff ?

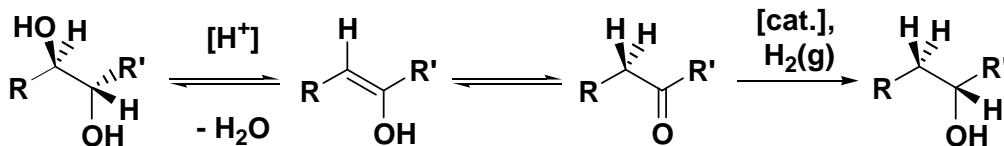


- **Controlled Acid (Brønstedt or Lewis) Catalyzed Dehydration.**
(*carbocations* → *thermodynamic bias for loss of secondary OH*)
- Hydrogenation and/or Hydrogenolysis of C=O, C=C, C-O & O-C=O.
- Thermodynamically “downhill” for all reactions.
- Iterative repetition in single reactor if required.
- Requires water- and acid-tolerant **homogeneous ionic hydrogenation/hydrogenolysis catalysts.**
- Advantage: no coking of catalyst surface with highly polar substrates

The Four Reactions for Catalytic Deoxygenation

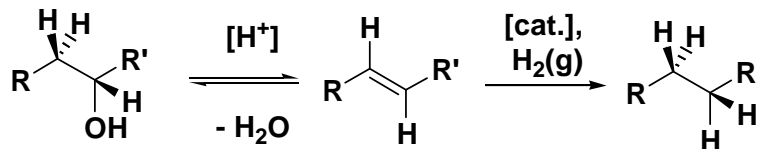
- Regardless of the source or target of the biomass deoxygenation the chemistry always involves only **four reaction types**.
- All are thermodynamically feasible and/or have been demonstrated with homogeneous catalysts.
- **Key:** catalysts must tolerate acid, water and fairly high temperatures.
- **Top choice:** highly chelated and robust electron poor group 8 metal (Fe, Ru) complexes.

1) Dehydration of *vic*-diols and hydrogenation of the resulting C=O double bond:



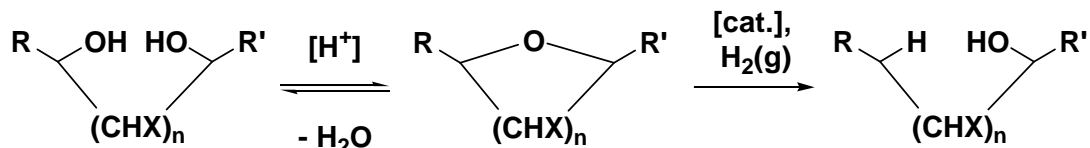
R = alkyl, hydroxy alkyl; R' = H, alkyl, hydroxy alkyl

2) Dehydration of alcohols and hydrogenation of the resulting C=C double bond:



3) Condensation of alcohols to oxacycles and hydrogenolysis of the resulting ether:

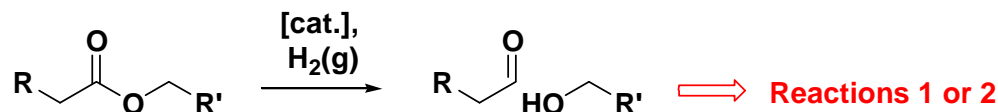
a) Direct Hydrogenolysis (thermodynamically possible but kinetically difficult)



X = H, OH, alkyl, aryl; n = 2,3,4

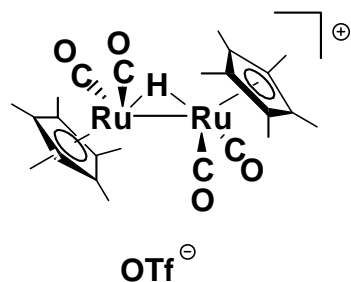
b) Easier: Rehydration, Loss of Water, Hydrogenation \rightleftharpoons **Reactions 1 or 2**

4) Hydrogenolysis of Esters

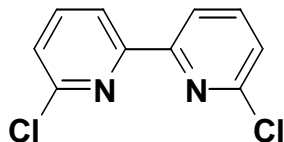
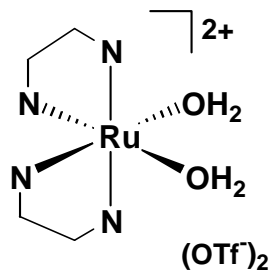


Types of Catalysts under Development @ Guelph

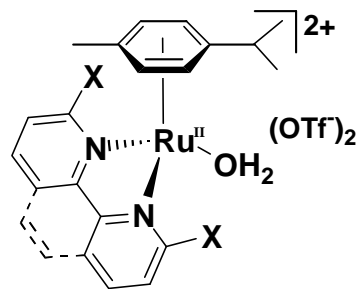
Time, money spent and # of grad students frustrated

BNL/DuPont Catalyst -
deactivated by water.

1



2

X = H, NH₂

3

coming to a
patent server
near you ...
(hopefully)

4

Catalyst	1 (1998)	2 (2004)	3 (2006)	4 (2008)
Temp. Limit [°C]	< 150	< 150	< 125	> 200
Diol ?	Yes	Yes	Yes	Yes
Alkanes from diols ?	No	Yes	Yes	Yes
Glycerol ?	< 1%	No	No	Maybe

1) US 6,555,717 & US 6,462,206. 2) Xie, Z.; Schlaf, M. *J. Mol. Catal. A: Chem.* **2005**, 229, 151-158. 3) Dykeman, R. R.; Luska, K. L.; Thibault, M. E.; Jones, M. D.; Schlaf, M.; Khanfar, M.; Taylor, N. J.; Britten, J. F.; Harrington, L. *J. Mol. Catal. A: Chem.* **2007**, 277, 233-251. 4) Thibault, M.E. & Schlaf, M.; Pending ...

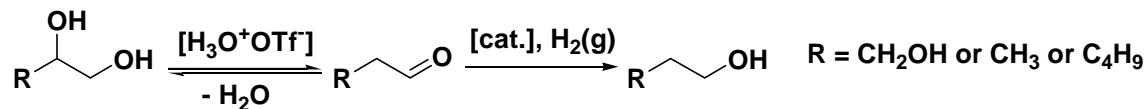
Example of a Catalyst in Action (Diol Model System)



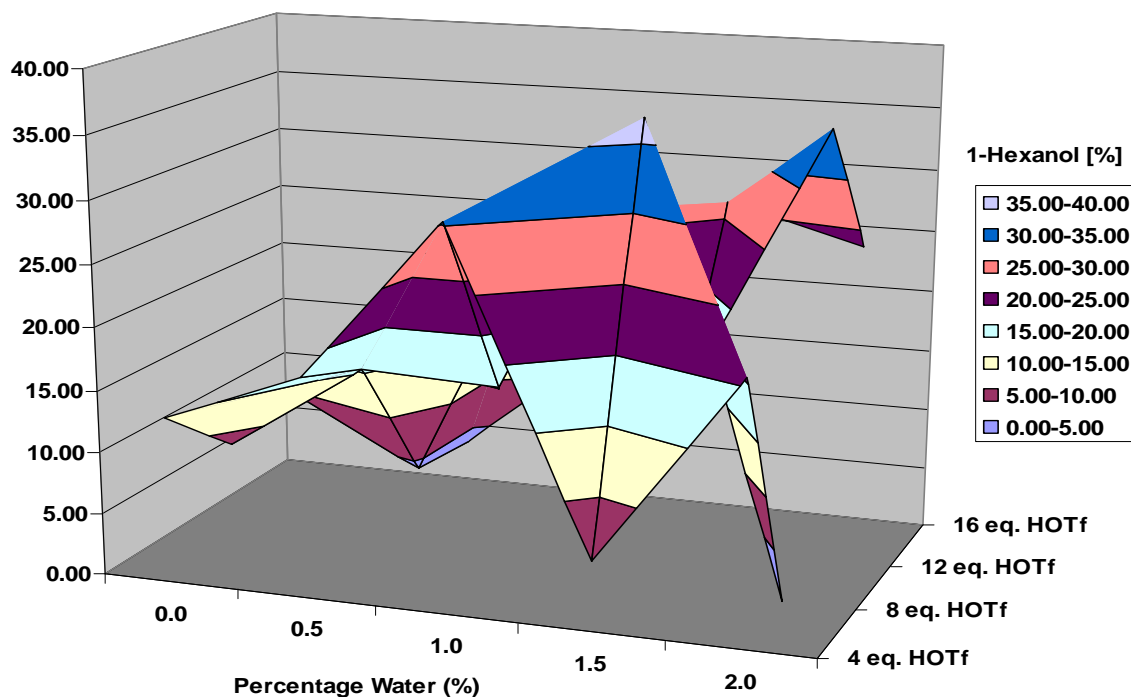
24 well parallel reactor
from HEL Group (UK)

Allows rapid screening of:
- various catalysts and/or
substrates.

- influence of two inter- or
independent reactant
concentrations on the
reaction outcome.



1,2-Hexanediol Deoxygenation with $[\text{Ru}(\text{p-cymene})(\text{Phen})(\text{H}_2\text{O})](\text{OTf})_2$



Reaction 1: Yield of 1-hexanol from 1,2-hexanediol with Ru-catalyst **3** as a function of acid/water concentration.

- **Dr. Anthony Clarke, Cell and Molecular Biology**
- **Dr. Hung Lee, Environmental Biology**
- **Dr. Amar Mohanty, Premier's Research Chair in Biomaterials**
- **Dr. Steven Rothstein, University Research Chair, Cell and Molecular Biology**
- **Dr. Peter Pauls, Plant Agriculture**
- **Dr. Marcel Schlaf, Chemistry**

- **Dr. Haridoss Sarma, Technology Transfer Mgr, Business Development Office**

- **Dr. Steven N. Liss, Associate Vice-President (Research Services)**
- **Prof. Rich Moccia, Associate Vice-President (Agri-Food Partnerships)**

- www.uoguelph.ca/research/
- www.uoguelph.ca/research/bdo/index.shtml